

# The role of anions on the Helmholtz Plane for the solid-liquid interface in aqueous rechargeable lithium batteries

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## ABSTRACT

The Li-ion transport at the electrode/electrolyte interface in lithium ion batteries (LIBs) relies on the structure of the electrical double layer. Our previous work indicates that the constructing of Janus amphiphilic coordination interface on LiFePO<sub>4</sub> in aqueous electrolyte relieves the energy barriers of the Li<sup>+</sup> solvation/desolvation process. Here, aqueous electrolytes with different salts (LiNO<sub>3</sub>, LiCl, Li<sub>2</sub>SO<sub>4</sub> and CH<sub>3</sub>COOLi) were tested in LiFePO<sub>4</sub> single nanoparticle, and Ab initio calculations and simulation were carried out. H<sub>2</sub>O has a stronger binding energy with Fe and Li on the surface of LiFePO<sub>4</sub> to form Janus interface, so the activation energies of Li-ion in Janus layer are the same in the four electrolytes. The simulation result confirms that the Li-ion transport at the interface have a close relationship with the anionic physical characteristics. Combing with the experimental and calculated results, it can be inferred that the activation energy ( $E_a$ ) of Li-ion includes Janus interface, anion adsorption layer and cation adsorption layer. Owing to the same Janus interface and cation adsorption layer, the difference of  $E_a$  in the four kinds of electrolytes must come from the anion adsorption layer in inner Helmholtz plane (IHP). This work provides a guiding significance on development of aqueous electrolyte systems.

## 1. Introduction

Incented by the ever-increasing demands of advanced energy storage systems for portable electronic devices and electric vehicles (EVs), the development of high-performance cathode materials for lithium ion batteries (LIBs) has attracted worldwide attentions. Consequently, the electrochemical properties and mechanisms of cathode materials have been extensively studied in the past decade. While most current studies in this area mainly focus on the macroscopic bulk crystal structure and properties, other previous studies suggest that the interfacial structures of materials largely dictates their electrochemical performances due to their unique electrical double layer formed at different chemical/electrochemical conditions. Electrical double layer (EDL) is always existence on electrode/electrolyte interface as an essential constituent, no matter whether there is solid electrolyte interphase (SEI) or not [1,2]. Helmholtz is one kind of the classical models in EDL, which includes inner Helmholtz plane (IHP) and outer Helmholtz plane (OHP). In general,

adsorbed ions or molecules are located in IHP and solvated adsorbed ions belongs to OHP [3]. The thin Helmholtz plane has a big influence on electrochemical performance, such as capacitor and LIBs, which has attracted a lot of attentions [4]. For example, Yan et al. investigated different adsorption species in IHP of Li-metal, which has great influence on diffusion of Li-ion from electrolyte to Li-metal surface [5]. Wang and Xu's group achieved high working voltage and improved cycle ability in aqueous Li-ion batteries by building a stable protecting layer on IHP [6, 7].

Our recent work found that replacing traditional organic electrolytes with aqueous electrolytes leads to different kinetics for ion intercalation and de-intercalation for LiFePO<sub>4</sub> LIBs [8,9]. By combining theoretical simulations with electrochemical characterization techniques in atomic/nano scales such as single-particle and mass-electrochemical measurements, microscopic information of the solid-liquid interfacial reactions has been obtained [10]. We found that the FeO<sub>6</sub> and LiO<sub>6</sub> octahedral structure units in crystal were symmetrically broken to

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become  $\text{FeO}_5$  and  $\text{LiO}_3$  units at surface, which interacted with solvent  $\text{H}_2\text{O}$  molecule to create both  $\text{FeO}_5(\text{H}_2\text{O})$  and  $\text{LiO}_3(\text{H}_2\text{O})_3$  octahedral reconstructive structure units (named as a “Janus” interface) at the EDL that relieves the energy barriers of the  $\text{Li}^+$  solvation/desolvation process, ultrafast rate performances can be achieved. At this point, one question has been aroused: what’s the role of anions on the formation of EDL in the aqueous electrolytes? Owing to the high structural stability and relatively low operating voltages, the surfaces of olivine materials are immune to side reactions compared to other cathode materials, such as Ni-rich layered cathode materials [11,12]. Though the final cathode material is covered by a thin carbon layer for high electronic conductivity, which has a loose structure with a large number of internal spaces, so the water molecules can permeate the carbon coat [9,13]. Therefore, the  $\text{LiFePO}_4$  system is still an ideal model to reveal the impact of anions on the interfacial properties of cathode materials [14].

In this work, we improved our previous single particle (SP) model to deal with a wider temperature scope to explore the role of anions in aqueous electrolytes. The quasi single particle (QSP) electrode of  $\text{LiFePO}_4$  was tested in different electrolytes (1 M  $\text{LiNO}_3$ , 1 M  $\text{LiCl}$ , 0.5 M  $\text{Li}_2\text{SO}_4$  and 1 M  $\text{CH}_3\text{COOLi}$ ) and different temperatures (0, 25 and 50 °C). By simulation and comparing the cyclic voltammogram (CV) curves of the four kinds of electrolytes, we found that the standard rate constant ( $k^0$ ) for Li-ion intercalation and de-intercalation inter has a strong relationship with the ionic radius: the bigger of ionic radius, the smaller of  $k^0$  value. Moreover, the interaction between anion and Li-ion is also important for Li-ion transport, such as  $\text{CH}_3\text{COOLi}$ , which owns the shortest radius but the transfer speed of Li-ion is slower compared with  $\text{LiNO}_3$  and  $\text{LiCl}$  owing to the strong interaction between  $\text{CH}_3\text{COO}^-$  and Li-ion. By ab initio calculations, we proved that not only  $\text{H}_2\text{O}$ , but also the anions can realize interface reconstruction and form octahedral structure in vacuum condition, but  $\text{H}_2\text{O}$  has priority in the real liquid environment. In aqueous electrolytes, anions will be absorbed next to the Janus  $\text{LiFePO}_4/\text{H}_2\text{O}$  inner Helmholtz plane (IHP) by electrostatic interaction, and the thickness of absorbed layer ( $d$  value) has a great influence on Li-ion transport between electrolyte and active materials. Finally, we separated the above four kinds of electrolytes into two group: fast-type electrolytes ( $\text{LiNO}_3$  and  $\text{LiCl}$ ) and slow-type ( $\text{Li}_2\text{SO}_4$ ,  $\text{CH}_3\text{COOLi}$ ), the former group owns smaller activation energy and little pre-exponential factor, which is beneficial for Li-ion transport between electrolyte and active material.

## 2. Experimental methods

### 2.1. Preparation of $\text{LiFePO}_4@\text{C}$

The  $\text{LiFePO}_4$  nanocrystals were synthesized by the normal method, mixing  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$  (AR, 99%),  $\text{H}_3\text{PO}_4$  (AR, 85% solution) and  $\text{LiOH}$ .  $\text{H}_2\text{O}$  (AR, 95%) in ethylene glycol (AR, 99%) according to a specific proportion, and the detailed processes are presented in our previous work [8].

### 2.2. Characterization

The crystal structure data of  $\text{LiFePO}_4@\text{C}$  was collected by X-ray diffraction (XRD, Bruker D8 Advance diffractometer with a Cu-K $\alpha$  radiation source). The morphology of  $\text{LiFePO}_4@\text{C}$  was investigated by a scanning electron microscopy (SEM, ZEISS SURPA 55).

### 2.3. QSP electrode preparation, and electrochemical measurements

Three electrode measurement was carried out to make clear the influence of anions on lithium ion interfacial transport. The working electrode was made up by mixing  $\text{LiFePO}_4$  nanocrystals (9 mg), carbon nano tube (6 mg), and Nafion solution (0.15 g, 5% concentration) into NMP (1.0 g) and ultrasound for a long time (more than 70 min). 60% PTFE solution is another binder used in our experiment. The final slurry

was dropped on the quartz monitor crystals and dried by air dry oven, then the working electrode formed, which was named as quasi single particle electrode (QSP electrode). The Ag/AgCl and platinum electrode were used as reference electrode and counter electrode, respectively. Then, we chose different salt dissolving in  $\text{H}_2\text{O}$  as the electrolyte, including 1 M  $\text{LiNO}_3$ , 1 M  $\text{LiCl}$ , 0.5 M  $\text{Li}_2\text{SO}_4$  and 1 M  $\text{CH}_3\text{COOLi}$ . Finally, the electrochemical performance of  $\text{LiFePO}_4$  QSP electrode measured in different electrolytes were collected by cyclic voltammetry (CV) measurements recorded by a CHI electrochemistry workstation (CHI604E).

### 2.4. Calculation method

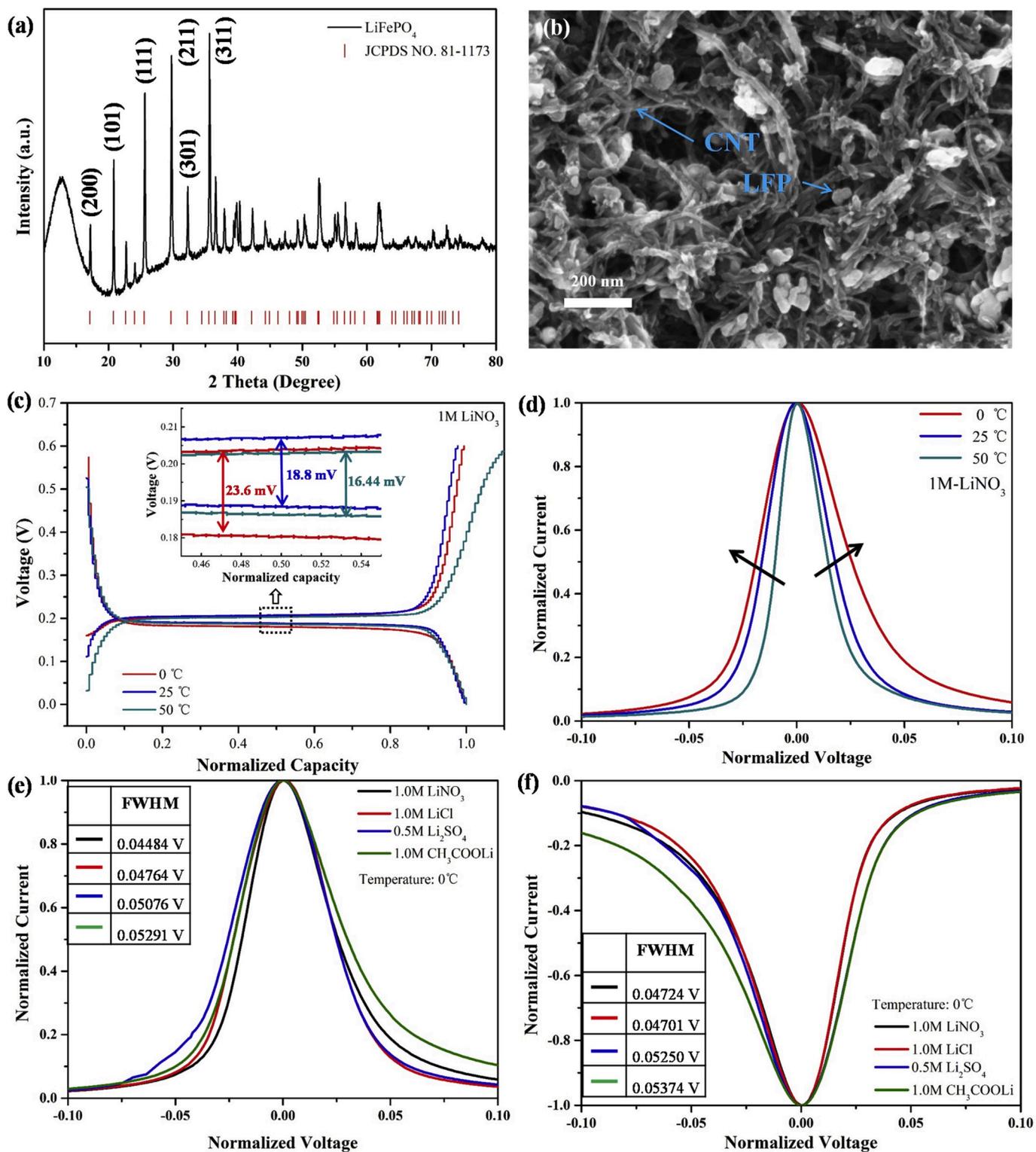
All calculation was performed using the first-principles density functional theory (DFT) calculations with the exchange–correlation energy functional, which were described by a generalized gradient approximation with the Perdew–Burke–Ernzerhof (PBE) exchange–correlation function [15]. To simulate  $\text{H}_2\text{O}$ ,  $\text{Cl}^-$ ,  $\text{NO}_3^-$  and  $\text{SO}_4^{2-}$  adsorbed on the  $\text{FePO}_4$  and  $\text{LiFePO}_4$  (0 1 0) surfaces, two ( $1 \times 1 \times 3$ ) supercell were used and enabled by a VASP code in which the projector augmented wave (PAW) method represented the electron–ion interaction with a kinetic energy cutoff of 520 eV [16,17]. The k-points were  $4 \times 2 \times 1$  for the supercell using the Monkhorst–Pack method [18]. During optimizations, the energy and force converged to  $10^{-4}$  eV per atom and  $0.01 \text{ eV } \text{Å}^{-1}$ , respectively. The spin = 2 polarization was used in all the calculations.

## 3. Results and discussion

### 3.1. Section I. Experimental results

The XRD pattern of  $\text{LiFePO}_4$  was collected, and all the diffraction peaks are fully indexed to the orthorhombic structure with Pnma(62) space group, consistent well with the standard peaks (JCPDS NO. 81–1173) as shown in Fig. 1a. Obviously, the final material is in pure phase without any impurity. According to our synthesis conditions (low temperature and reduction reaction environment) and some relevant works [19,20], the tiny amount of  $\text{Fe}_2\text{P}$  and  $\text{FeOx}$  impurities can be excluded. Combining with Scherrer equation  $D = K \lambda / \beta \cos \theta$  ( $K$  is a dimensionless shape factor,  $\lambda$  is the XRD wavelength,  $\beta$  is the line broadening at half the maximum intensity (FWHM),  $\theta$  is the Bragg angle) and the strongest peak (311), the mean particle size of  $\text{LiFePO}_4$  was calculated to be about 46.22 nm. Fig. S1 shows the SEM images of  $\text{LiFePO}_4$  with a mean size about 40–50 nm, consistent with the calculated results by Scherrer equation. We scattered the  $\text{LiFePO}_4$  nano-particles in carbon nanotube (CNT) network, and treat it with ultrasonic by a long time (longer than 70 min). The detailed experimental process can be found in our previous work [8]. The above slurry was dropped on the quartz monitor crystals and dried in the air dry oven, which was named as quasi single particle (QSP) electrode. Fig. 1b shows the distribution situation of  $\text{LiFePO}_4$  nano-particles and CNT on the QSP electrode, obviously, the  $\text{LiFePO}_4$  particles were completely dispersed into the NCT network, which can minimize the concentration polarization, electrochemical polarization, and other internal interference.

It’s well known that impurity phase (especially for  $\text{Fe}_2\text{P}$ ) is easy to be generated during synthesis of  $\text{LiFePO}_4$  [21,22], which can be easily detected by XRD and TEM. Thus, TEM measurements were performed to detect the possibility of impurity phase on the surface of our synthesized  $\text{LiFePO}_4$ . As shown in Figs. S2a and S2b, there is no signal of the existence of impurity phase on the  $\text{LiFePO}_4$  particle surface, consistent with our XRD results and our previous work (Figs. S2c and S2d) [23]. This indicates the clean surface of our material. Previous works using the same synthesis method as ours also reported that no relevant impurities were detected [24,25]. For example, the work by William’s group studied Li-ion diffusion on the surface of  $\text{LiFePO}_4$  in aqueous electrolyte [14] and showed the same surface structure of  $\text{LiFePO}_4$  as we did, and no



**Fig. 1.** (a) The XRD data of LiFePO<sub>4</sub>. (b) SEM image of the QSP electrode, obviously, the electrode materials scattered very well in the CNT network. (c) Charge-discharge curves of the QSP electrode in 1 M LiNO<sub>3</sub> at different temperature at 0.1C, the inserted picture is partial enlarged detail of c, which shows us the polarization voltage in different temperature. (d) The normalized CV curves of the LiFePO<sub>4</sub> QSP electrode measured in 1 M LiNO<sub>3</sub>. (e and f) The difference of normalized CV curves measured in different electrolytes at 0 °C, the Full Width at Half Maximum (HWHM) data of each curves are listed and inserted into (e) and (f).

impurity phases was detected on the facet other than the coated carbon.

Charge-discharge curves of LiFePO<sub>4</sub> in different electrolytes and temperatures were collected and shown in Fig. 1c and S3. The corresponding voltage interval and current density are 0–0.6 V and 0.1 C. As for 1 M LiNO<sub>3</sub>, the voltage difference between charge-discharge

platforms changed by a little content from 0 °C to 50 °C, which are 20.9 mV (0 °C), 17 mV (25 °C) and 16.9 mV (50 °C) (Fig. 1c). Under a certain condition, high temperature is helpful for Li-ion diffusion both in material and electrolyte, so the polarization phenomenon (platform difference) is weakened. LiFePO<sub>4</sub> tested in 1 M LiCl, 0.5 M Li<sub>2</sub>SO<sub>4</sub> and 1

M CH<sub>3</sub>COOLi also owns the same phenomenon, as shown in Fig. S3. Furthermore, cyclic voltammetry (CV) measurements were carried out in the above four kinds of electrolytes under different temperatures. Fig. 1d, S4 and S5 presents the normalized CV curves both in charge and discharge processes, which become narrower with the increase of temperature. For LiNO<sub>3</sub> electrolyte, the normalized FWHMs of the CV curves are 0.045V, 0.034V, and 0.0225V from 0 °C to 50 °C (Fig. 1d). In order to compare the differences of Li-ion transport in different electrolytes and different temperatures, we put the CV curves measured at the same temperature together and carried out normalization, as shown in Fig. 1e, f and S6. When tested at 0 °C, the FWHMs of CV curves in different electrolytes are different, and the peak of 1 M LiCl and 1 M LiNO<sub>3</sub> are the narrowest. The FWHMs of normalized CV curves during charge processes are 0.04484V (LiNO<sub>3</sub>), 0.04764V (LiCl), 0.05076V (Li<sub>2</sub>SO<sub>4</sub>) and 0.05291V (CH<sub>3</sub>COOLi), and the corresponding FWHMs during discharge processes are 0.04724V, 0.04701V, 0.05250V and 0.05374V (Table inserted into Fig. 1e and f). When the testing temperature increased to 50 °C, the difference of FWHMs are not so big compared with it tested in 0 °C, but CV curves are always the narrowest in LiCl and LiNO<sub>3</sub> (Figs. S6c and S6d). To exclude the affection of binder, we also prepared QSP LiFePO<sub>4</sub> electrode with PTFE binder. The new QSP electrode presents the same trends compared with the QSP electrode with Nafion binder (Fig. S7). Interestingly, with the same solution concentration and temperature, why CV curves show different FWHMs in aqueous electrolytes with different salts? With the same electrodes (working, counter and reference) used in all test systems, electrolytes are the only difference during the electrochemical tests. To clarify the reason accounting for the polarization difference, ionic conductivities of the four kinds of salts in H<sub>2</sub>O were measured (Fig. S8). The corresponding conductivities of LiNO<sub>3</sub>, LiCl, Li<sub>2</sub>SO<sub>4</sub> and CH<sub>3</sub>COOLi are 69, 74.18, 50.16 and 32.73 mS/cm at 25 °C, respectively. Obviously, the ionic conductivities of the four electrolytes are super higher than that in LiFePO<sub>4</sub> bulk with 10<sup>-9</sup> S/cm [26], so the ionic conductivities in the electrolyte should not be the decisive step. Thus, the polarization difference must come from the different solid-liquid interfaces (Helmholtz layer) formed between LiFePO<sub>4</sub> and different aqueous electrolytes. Moreover, The Li<sup>+</sup> transference numbers (*t*) of 1 M LiNO<sub>3</sub>, LiCl, Li<sub>2</sub>SO<sub>4</sub> and CH<sub>3</sub>COOLi aqueous electrolytes were calculated as shown in Fig. S8.

### 3.2. Section II. SP model and simulation results

We further performed electrochemical simulations to support the above inference. As we all know, Butler–Volmer (BV) model was usually selected to simulate and analyze the CV curves to get the transfer mechanism. However, it failed when used in two phase LiFePO<sub>4</sub> system [8]. However, in our previous model, a hypothesis was set that the whole Li-ion transfer processes would not stop in transitive state (Li<sub>x</sub>FePO<sub>4</sub>), owing to the fast transfer reaction between LiFePO<sub>4</sub> and FePO<sub>4</sub>. That's to say, there are only two phase transformation in the whole processes. However, we found that the CV peak become wider under aqueous electrolyte in low temperature, and the old model failed to simulate the CV curves in which the interfacial reaction would be influenced by temperature. This can be attributed to the different transport characteristics of lithium ion at solid-liquid interface from that of our previous electrochemical systems. The different transport characteristic brought new transitive state, which is different with the previous Li-ion transport behavior. When the testing condition was changed (e. g., temperature), the previous model will be unsuitable in low temperature because transitive phase appears and cannot be ignored. It's necessary to develop an innovative and reasonable model to realize more smart simulation to fit widely various conditions.

First, we know that the charge-discharge process of LiFePO<sub>4</sub> is a partially dissoluble two-phase process as shown in the following equation:



Note that the reaction rate is directly proportional to the surface concentration of FePO<sub>4</sub> and LiFePO<sub>4</sub>. Define the concentration of LiFePO<sub>4</sub> and FePO<sub>4</sub> at the surface are  $C_O(0, t)$  and  $C_R(0, t)$ . Then the current is determined by the rate of the reactant transmitted to the electrode surface. The net current of the whole reaction is:

$$i = nFA' [k_f C_O(0, t) - k_b (C_R(0, t))] \quad (2)$$

( $k_f$  is the heterogeneous reduction rate constant,  $k_b$  is the heterogeneous oxidation rate constant,  $F$  is Faraday constant,  $n$  is quantity of exchange electron,  $A'$  is specific interfacial surface area.)

The rate constant at different potential can be represented by the standard heterogeneous rate constant  $k^0$ , such as equations (3) and (4).

$$k_f = k^0 \exp \left[ -aF/RT (E - E^{\theta'}) \right] \quad (3)$$

$$k_b = k^0 \exp \left[ (1 - a)F/RT (E - E^{\theta'}) \right] \quad (4)$$

The novelty of the modified SP model is that the Li-ion de-intercalation/intercalation process of LiFePO<sub>4</sub>/FePO<sub>4</sub> was divided into three stages according to the charge/discharge curves (taking discharge as an example, as shown in Fig. 2a). The first stage is the high voltage part (Part I in Fig. 2a), which contains a small amount of Li-ion in FePO<sub>4</sub> (Li<sub>x</sub>FePO<sub>4</sub>;  $0 < x < b$ ,  $b \approx 0.1$ ). In this stage, we assume that  $k^0$  remain the same,  $k_f$  and  $k_b$  is calculated by FePO<sub>4</sub> using equations (3) and (4). The second stage is two phase coexistence stage (FePO<sub>4</sub> & LiFePO<sub>4</sub>;  $b \approx 0.1$ ,  $B \approx 0.9$ ), the value of  $b$  and  $B$  can be determined from the inflection point of the charge-discharge curve (Part II in Fig. 2a), and  $k_f$  and  $k_b$  are calculated according to the mixed value of LiFePO<sub>4</sub> and FePO<sub>4</sub>. In order to describe the process, we set a formal potential  $E$ , which presents the activation energy voltage. To get the formal potential ( $E$ ), which is a parameter that need to be identified, we first get the formal potential at the first stage ( $E_L$ ) and the third stage ( $E_H$ ), and then get the  $k_f$  and  $k_b$  in the second stage using the following equations (5) and (6).

$$k_f = k^0 \exp \left[ (-\alpha)F/RT \left( V(E - E_H + E_L)/E - E_L \right) \right] \quad (5)$$

$$k_b = k^0 \exp \left[ (1 - \alpha)F/RT \left( V(E - E_H + E_L)/E - E_L \right) \right] \quad (6)$$

$V$  is the scan voltage in the second stage.

The third stage is LiFePO<sub>4</sub> with some lithium vacancies (Li<sub>x</sub>FePO<sub>4</sub>;  $B < x < 1$ ). In this stage, we assume that  $k^0$  remain the same,  $k_f$  and  $k_b$  is calculated by FePO<sub>4</sub> using equations (3) and (4).

In the new model, lithium transport process as was divided in two parts, the diffusion process and interface charge transfer process. During the oxidation or reduction process, the Li-ions in LiFePO<sub>4</sub> will diffuse along the transport channel, and the diffusion process satisfies the diffusion law in spherical particle, as shown in Equation (7).

$$\frac{\partial C}{\partial t} = D_{Li} \frac{\partial^2 C}{\partial r^2} + 2 \frac{D_{Li}}{r} \frac{\partial C}{\partial r} \quad (7)$$

$D_{Li}$  is the diffusion coefficient of Li-ion,  $r$  is the radius of the nano LiFePO<sub>4</sub> particle.

Equation (3) and (4) can be brought into equation (2) to obtain the complete current (i)-electric potential ( $E$ ) relation expression. The interface electron exchange process of QSP electrode is described by the following equation.

$$i = FA' k^0 \left[ C_O(0, t) e^{-\alpha f(E - E^{\theta'})} - C_R(0, t) e^{(1 - \alpha) f(E - E^{\theta'})} \right] \quad (8)$$

in equation (8),  $f$  equals to  $F/RT$ .

Combining boundary conditions of the above equations, and using finite element method to calculate equations (7) and (8), we can obtain

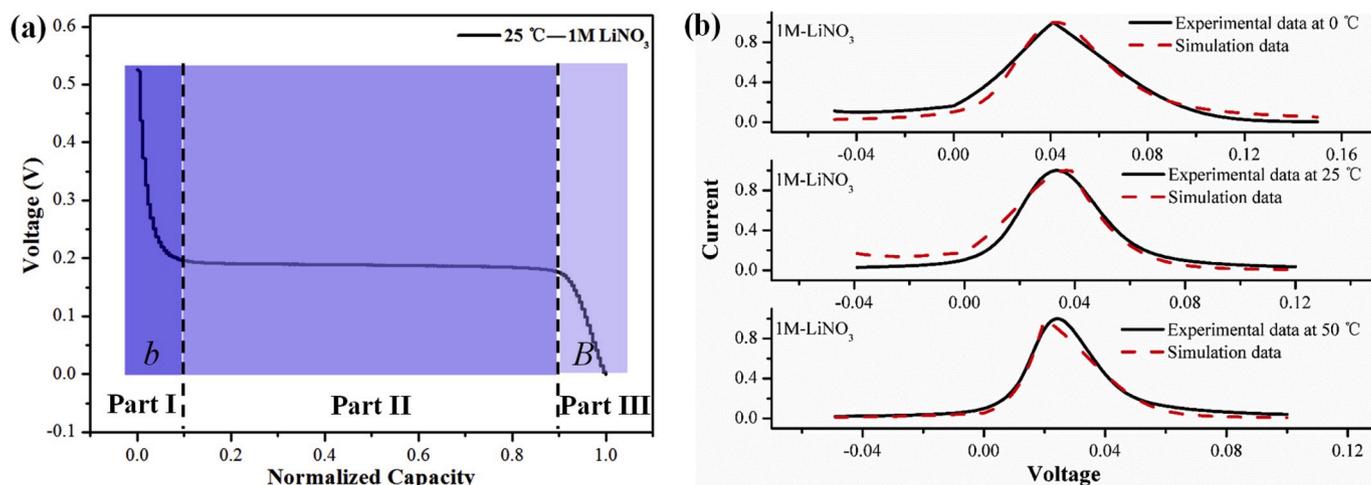


Fig. 2. (a) The normalized discharge curve of QSP electrode measured in 1 M LiNO<sub>3</sub>, which was divided into three parts for convenience of simulation. (b) The CV curves of QSP electrode tested in 1 M LiNO<sub>3</sub> at different temperature, the dotted lines are the simulation curves by the updated SP-model.

Li-ion kinetic parameters both in bulk and surface.

As shown in Fig. 1e, f and S6, LiFePO<sub>4</sub> QSP electrodes presented different electrochemical behaviors in 1 M LiNO<sub>3</sub>, 1 M LiCl, 0.5 M Li<sub>2</sub>SO<sub>4</sub>, or 1 M CH<sub>3</sub>COOLi at different temperatures. We simulated the testing data by the modified SP-model through changing the parameter of  $k^0$ ,  $\alpha$ ,  $D_{Li}$  and  $E$  in this model, good fitting results were obtained, as shown in Fig. 2b and S9. The simulation results of  $k^0$  are shown in Fig. 3a and b  $k^0$  increases with the increase of testing temperature and  $k^0$  at charge (Li-ion de-intercalation) is smaller about 60% than that at

discharge (Li-ion intercalation), and this trend exists in all four kinds of electrolytes. However, at a certain temperature, the exact values of  $k^0$  are different in the four kinds of electrolytes. The rate constant  $k^0$  in LiNO<sub>3</sub> and LiCl solution are higher than in Li<sub>2</sub>SO<sub>4</sub> and CH<sub>3</sub>COOLi. In order to facilitate comparing the differences, the electrolytes were divided into two types: the fast-type (LiNO<sub>3</sub> and LiCl) and the slow-type (Li<sub>2</sub>SO<sub>4</sub> and CH<sub>3</sub>COOLi) according to the simulated data of  $k^0$ .  $k^0$  in the fast-type is larger than that in the slow-type (Fig. 3a and b). We calculated  $E_a$  and  $A$  by interface kinetic Arrhenius equation ( $\ln k^0 = \ln A - E_a/RT$ )

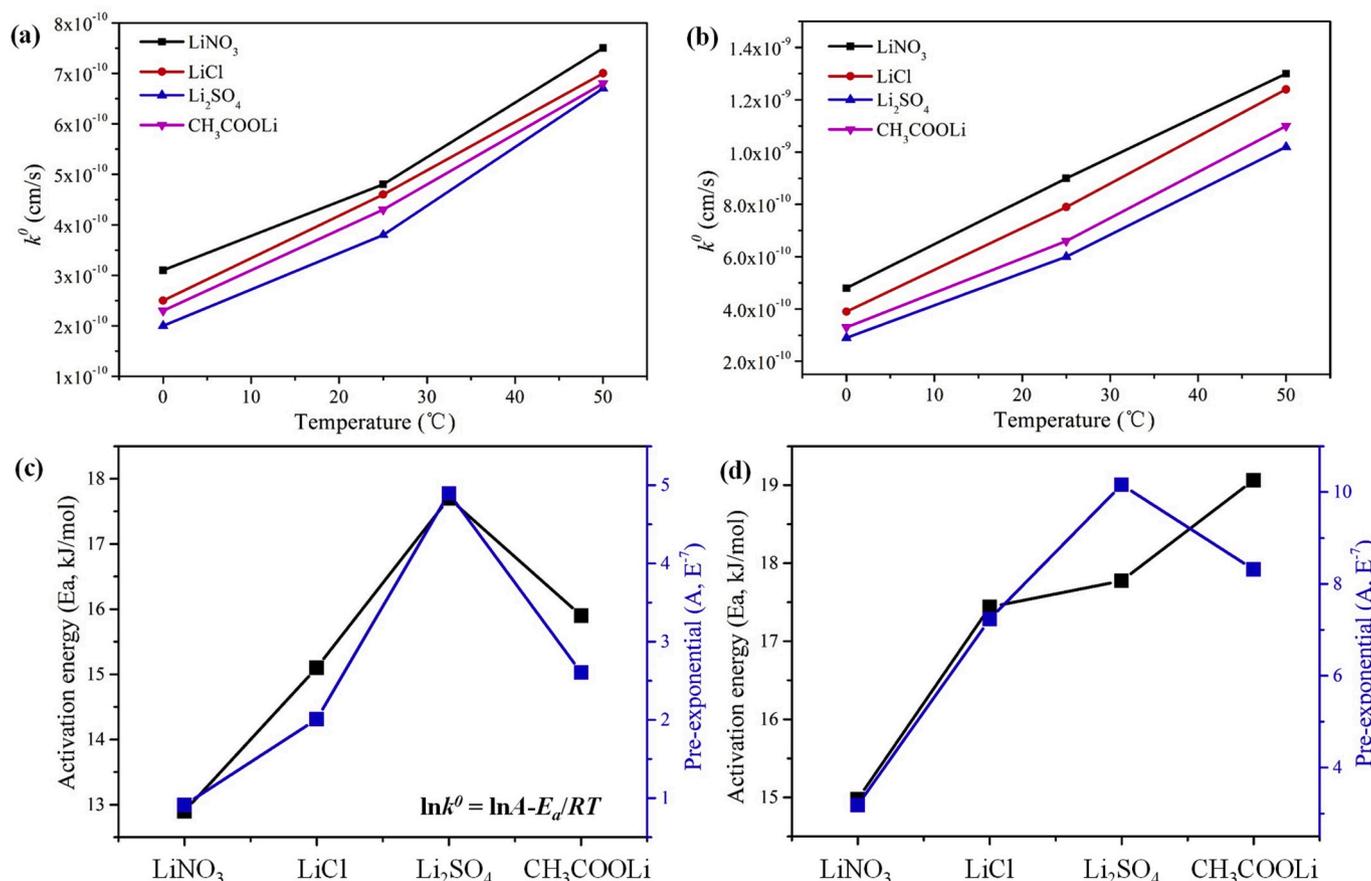


Fig. 3. The relationship between standard rate constant ( $k^0$ ) and temperature ( $T$ ) in different electrolytes during (a) charge and (b) discharge processes. Activation energy ( $E_a$ ) and pre-exponential ( $A$ ) of LiFePO<sub>4</sub> in different electrolytes, calculated by Arrhenius equation during (c) charge and (d) discharge processes.

$RT, k^0$  is the rate constant,  $E_a$  is activation energy,  $A$  is pre-exponential factor,  $R$  is molar gas constant,  $T$  is thermodynamic temperature), and the final results were shown in Fig. 3c and d. The detailed simulation processes and data of  $E_a$  and  $A$  were listed in Figs. S10 and S11. Obviously, the fast-type electrolytes owns smaller  $E_a$  and  $A$  compared with the slow-type electrolytes for Li-ion transport, indicating that the shorter jump distance and lower energy for Li-ion transport across the interface between electrolyte and electrode. Thus, our electrochemical simulations proved that the different polarizations in aqueous electrolytes with different salts indeed come from the different Helmholtz layer formed between  $\text{LiFePO}_4$  and different aqueous electrolytes, leading to different activation energies and jump distances for Li-ion transport across the Helmholtz layer.

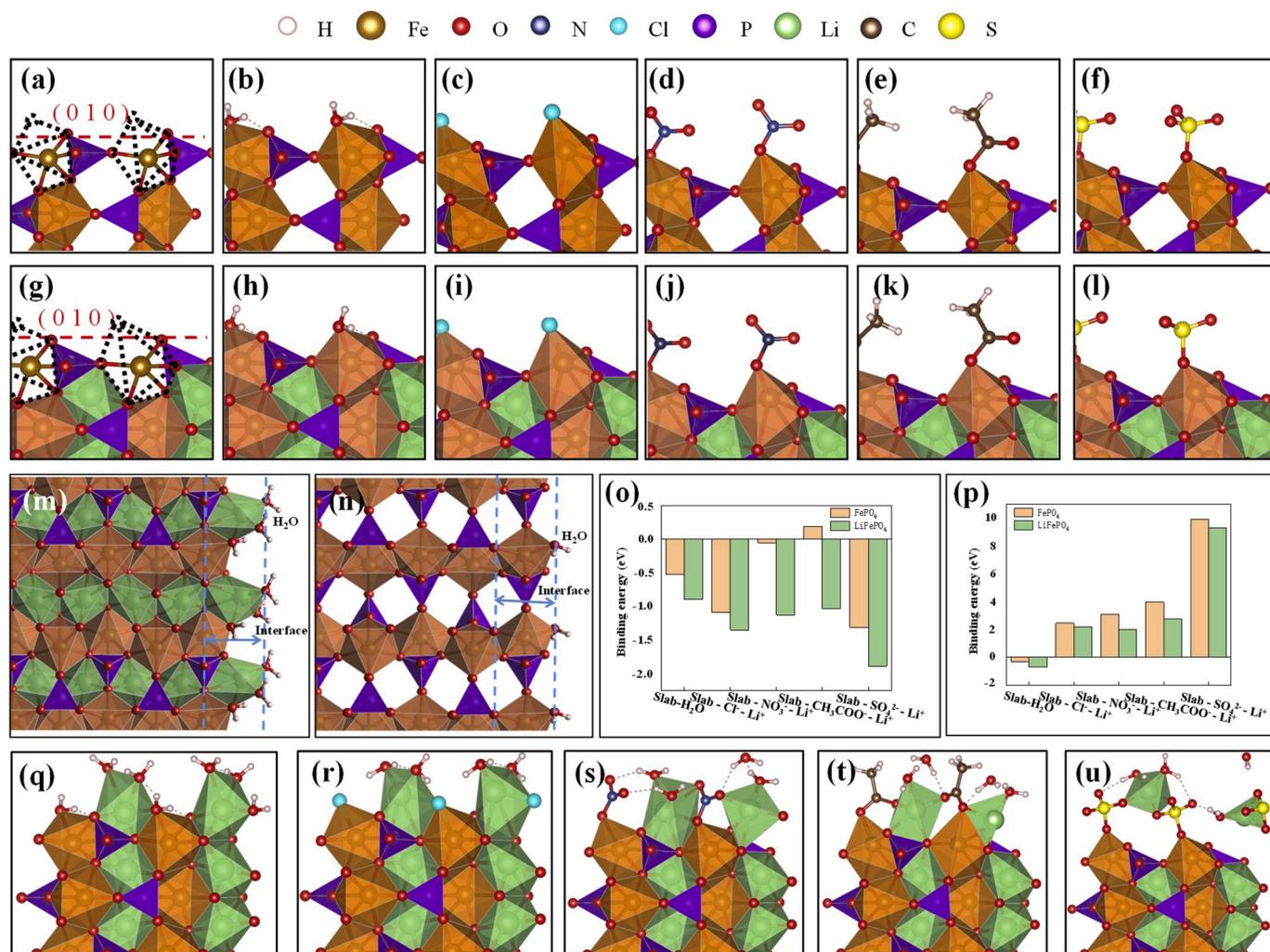
### 3.3. Section III. Density functional theory (DFT) calculation

In order to get an atomic cognition of the Helmholtz layer between  $\text{LiFePO}_4$  and different aqueous electrolytes, a broader DFT study was carried out to explore the coordination environment of anions on the surface of  $\text{LiFePO}_4$  and  $\text{FePO}_4$ . The interaction between the surface and the adsorbed species were calculated using basic ion pair model, Slab-

$\text{A}^{\text{n-}} - \text{nLi}^+$  model, where  $\text{A}^{\text{n-}}$  represents the anions adsorbed ( $\text{Cl}^-$ ,  $\text{NO}_3^-$ ,  $\text{CH}_3\text{COO}^-$  and  $\text{SO}_4^{2-}$ ). In the Slab -  $\text{A}^{\text{n-}} - \text{nLi}^+$  model, the  $\text{A}^{\text{n-}}$  was allowed to relax on the slab and the  $\text{Li}^+$  was fixed in the vacuum [5]. The binding energy ( $\Delta E_b$ ) was defined as follows:

$$\Delta E_b = E(i^*) - E(*) - E(i)$$

where  $E(i^*)$  and  $E(*)$  is the energy of the adsorption model and pristine surface respectively, and  $E(i)$  is the energy of ion pair  $i$  ( $\text{A}^{\text{n-}} - \text{nLi}^+$ ) or neutral molecule ( $\text{H}_2\text{O}$ ). The geometrical structures and binding energies of these interactions are summarized in Fig. 4. Fig. 4a and g shows the pristine (010) surface of  $\text{FePO}_4$  and  $\text{LiFePO}_4$ , which is an incomplete  $\text{FeO}_6$ -octahedral structure (to become  $\text{FeO}_5$ ), in which one "O-atom" is missed due to symmetric breaking from 3D bulk crystal to 2D surface. The O-atom of  $\text{H}_2\text{O}$  and anions (or  $\text{Cl}^-$ ) can place the missed "O-atom" on the surface of  $\text{FePO}_4/\text{LiFePO}_4$  (010), and formed stable reconstructed octahedral structure as shown in Fig. 4a-l. According to our previous work, the detailed interface structure built by  $\text{H}_2\text{O}$  on the surface of  $\text{LiFePO}_4$  and  $\text{FePO}_4$  are shown in Figure 4m and n. Generally, the  $\text{LiFePO}_4$  slab affords a much larger binding energy towards ions than  $\text{FePO}_4$ . The large binding energies of anions are induced by the as-



**Fig. 4.** (a) The structure of (0 1 0) surface of  $\text{FePO}_4$  with (b)  $\text{H}_2\text{O}$  adsorbed, (c)  $\text{Cl}^-$  adsorbed, (d)  $\text{NO}_3^-$  adsorbed, (e)  $\text{CH}_3\text{COO}^-$  adsorbed and (f)  $\text{SO}_4^{2-}$  adsorbed. (g) The structure of pristine (0 1 0) surface of  $\text{FePO}_4$ . (h)  $\text{H}_2\text{O}$  adsorbed, (i)  $\text{Cl}^-$  adsorbed, (j)  $\text{NO}_3^-$  adsorbed, (k)  $\text{CH}_3\text{COO}^-$  adsorbed and (l)  $\text{SO}_4^{2-}$  adsorbed. (m, n) the detailed Janus solid-liquid interface structure of  $\text{LiFePO}_4$  and  $\text{FePO}_4$  built by  $\text{H}_2\text{O}$ . (o) The binding energies of the Slab- $\text{H}_2\text{O}$  and Slab-Anion- $\text{Li}^+$  models of  $\text{FePO}_4$  and  $\text{LiFePO}_4$ . (p) The binding energies with de-solvation energy taken into consideration of the Slab- $\text{H}_2\text{O}$  and Slab-Anion- $\text{Li}^+$  models of  $\text{FePO}_4$  and  $\text{LiFePO}_4$ . The structure of "Janus" solid-liquid interface reconstructed by  $\text{Li}^+$  ( $\text{H}_2\text{O}$ )<sub>2</sub> on (010) surface of  $\text{LiFePO}_4$  with (q)  $\text{H}_2\text{O}$ , (r)  $\text{Cl}^-$ , (s)  $\text{NO}_3^-$ , (t)  $\text{CH}_3\text{COO}^-$  and (u)  $\text{SO}_4^{2-}$  adsorption.

formed strong Fe–O/Cl interactions as well as a significant charge transfer. It is obvious that some of  $\text{Cl}^-$ ,  $\text{NO}_3^-$ ,  $\text{CH}_3\text{COO}^-$  and  $\text{SO}_4^{2-}$  could bind with  $\text{LiFePO}_4$  or  $\text{FePO}_4$  slab spontaneously (Figure 4o). However, the interface reconstruction energy in different coordination environment are different with the influence of solvent water taken into consideration. The binding energy ( $\Delta E_b$ ) includes de-solvation energy ( $E_{i,\text{desol}}$ ) were defined as follows:

$$\Delta E_b = E(i^+) - E(*) - (E(i) - E_{i,\text{desol}})$$

With  $E_{i,\text{desol}}$  of  $\text{H}_2\text{O}$  and anions [27,28] taken into consideration, the  $\Delta E_b$  of  $\text{Cl}^-$ ,  $\text{NO}_3^-$ ,  $\text{CH}_3\text{COO}^-$  and  $\text{SO}_4^{2-}$  all turn into positive (1.99–9.92 eV, Figure 4p). The results illustrate that it's a spontaneous process for  $\text{H}_2\text{O}$  to finish the octahedral interface reconstruction with Fe, as for the four kinds of anions, need external influence to construct perfect Janus-interface. So, in the aqueous electrolyte system,  $\text{H}_2\text{O}$  has absolute advantage to achieve interface reconstruction compared with the mentioned anions. The detailed Janus interface forming mechanism and interface charge transfer processes were shown in Fig. S12. Li-ions ( $\text{Li}^+(\text{H}_2\text{O})_4$ ) diffusion processes on the surface of  $\text{FePO}_4$  needs to detach two water molecules to come to the surface owing to the Janus solid–liquid interface [8]. The structure of Janus solid–liquid interface built by  $(\text{Li}^+(\text{H}_2\text{O})_2)$  on (010) surface of  $\text{LiFePO}_4$  with  $\text{H}_2\text{O}$ ,  $\text{Cl}^-$ ,  $\text{NO}_3^-$ ,  $\text{CH}_3\text{COO}^-$  and  $\text{SO}_4^{2-}$  adsorption were shown in Fig. 4q–u. According to this, we calculated the energy changing curve of Li-ion embedding using the climbing image nudged elastic band method [29]. The migration energy barriers of Li-ion transfer from surface to bulk in different electrolytes under vacuum condition are different as shown in Fig. 4q–u, which are 0.27 eV ( $\text{H}_2\text{O}$ ), 0.90 eV ( $\text{Cl}^-$ ), 0.84 eV ( $\text{NO}_3^-$ ), 0.94 eV ( $\text{CH}_3\text{COO}^-$ ), and 1.01 eV ( $\text{SO}_4^{2-}$ ). That's to say, anion diversity has a big influence on Li-ion solvation-desolvation process in vacuum environment.

Combine with the above calculation and analysis, obviously, in aqueous electrolyte  $\text{H}_2\text{O}$  will connect with Fe and form Fe–O octahedral structure and Janus interface (Fig. 5a). Obviously, the EDL on the surface of  $\text{FePO}_4$  or  $\text{LiFePO}_4$  includes Janus interface, anion adsorption layer and cation adsorption layer as shown in Fig. 5a, which has been described by Newman and Thomas-Alyea [3]. There is only one kind of cation in the above electrolytes, which is Li-ion, so the cation adsorption layer in the four kinds of interfaces should be the same. Hence, the difference of CV curves in different aqueous electrolytes must come from anions. The ionic radius and charge quantity of  $\text{NO}_3^-$ ,  $\text{Cl}^-$ ,  $\text{SO}_4^{2-}$ , and  $\text{CH}_3\text{COO}^-$  are different, which are 1.79 Å for  $\text{Cl}^-$ , 1.84 Å for  $\text{NO}_3^-$ , 1.62 Å

for  $\text{CH}_3\text{COO}^-$  and 2.58 Å for  $\text{SO}_4^{2-}$ , so the size of the anions group (connected with  $\text{H}_2\text{O}$ ) are different. The bigger of the anion group, the higher of activation energy for Li-ion realizing solvation-desolvation processes, because Li-ion needs a longer jump distance from electrolyte to the Janus interface ( $d$  in Fig. 5a). As for  $\text{CH}_3\text{COO}^-$ , owns a small radius but needs higher Li-ion activation energy, which can be indexed to the strong appetency with Li-ion (weak electrolyte). This should be the reason why the interfacial rate constant ( $k^0$ ) and  $E_a$  in different electrolytes are different. Actually, the reconstruction layer and adsorbed layer were belonged to Helmholtz Plane, and named as IHP and OHP as shown in Fig. 5b. IHP includes adsorbed molecules (Janus interface) and ions (anion adsorption layer), while solvated adsorbed ions (cation adsorption layer) are located in OHP.  $E_0$ ,  $E_1$  and  $E_2$  represent the activation energies related to IHP ( $E_0+E_1$ ) and OHP ( $E_2$ ), and the summation of  $E_0$ ,  $E_1$  and  $E_2$  equals to activation energy  $E_a$  shown in Fig. 3c and d. Herein, owing to the spontaneously reconstruction process between  $\text{H}_2\text{O}$  and  $\text{FePO}_4$ , the value of  $E_0$  in the four electrolytes should be the same. Moreover,  $E_2$  should be the same in the four kinds of interfaces, because of the single kind of cation. So the difference of  $E_a$  can be attributed to the difference of  $E_1$  (anion adsorption layer), which owns the same variation trend compared with  $E_a$  as shown in Fig. 5b. Hence, it's easier for Li-ion passing through the Helmholtz Plane in  $\text{LiNO}_3$  and  $\text{LiCl}$  electrolytes compared with it in  $\text{Li}_2\text{SO}_4$  and  $\text{CH}_3\text{COOLi}$ , owing to the small  $E_1$  in IHP.

#### 4. Conclusions

In this work, we prepared SP electrode of  $\text{LiFePO}_4$ , and did CV testing in different aqueous electrolytes (1 M  $\text{LiNO}_3$ , 1 M  $\text{LiCl}$ , 0.5 M  $\text{Li}_2\text{SO}_4$ , and 1 M  $\text{CH}_3\text{COOLi}$ ) and different temperatures. Interestingly, differences were found in the CV curves between the four electrolytes, especially when the testing temperature was decreased. Combining with the improved SP model, the accurate interfacial rate constant  $k^0$  and activation energy  $E_a$  in the four kinds of electrolytes were obtained. Ab initio calculations proved that it's easier for  $\text{H}_2\text{O}$  realizing octahedral interface reconstruction compared with  $\text{NO}_3^-$ ,  $\text{Cl}^-$ ,  $\text{SO}_4^{2-}$  and  $\text{CH}_3\text{COO}^-$ , so the reconstruction interface (Janus interface with both  $\text{FeO}_5(\text{H}_2\text{O})$  and  $\text{LiO}_3(\text{H}_2\text{O})_3$  octahedral reconstructive structure units) in the four kinds of electrolytes are the same. The activation energy of Li-ion from electrolyte to electrode includes three parts, which are Janus interface (IHP), anion adsorption layer (IHP) and cation adsorption layer (OHP). Owing to the same Janus interface and cation adsorption layer, the difference of

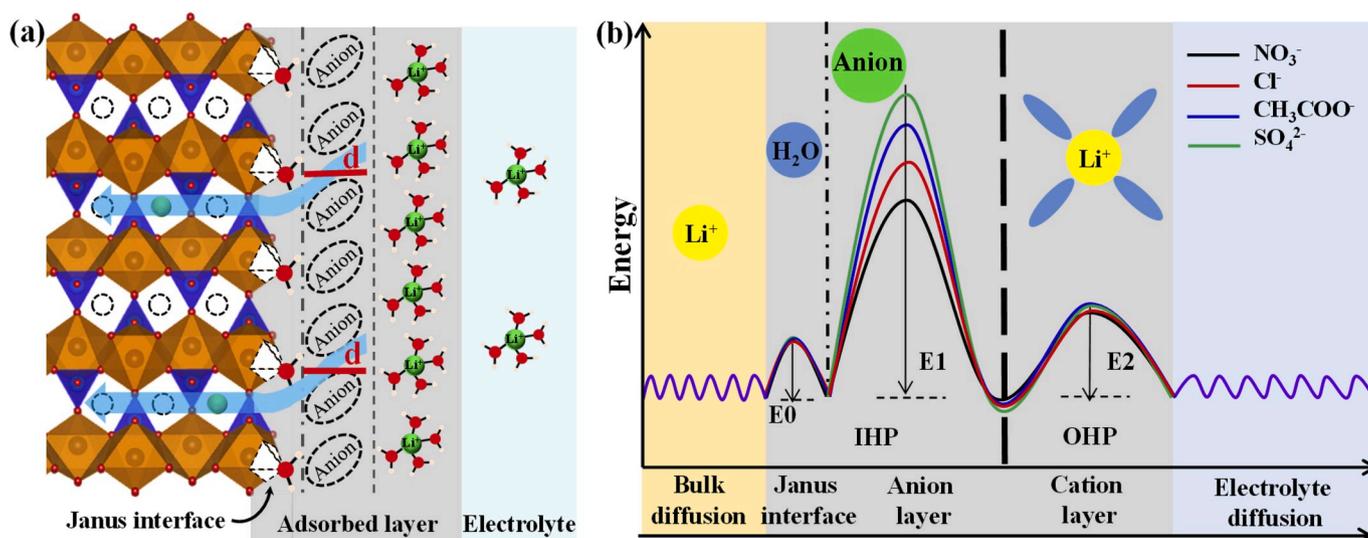


Fig. 5. (a) Schematic descriptions of the effect of anion on Li-ion transport from electrolyte to electrode. (b) The relationship of migration energy barrier of  $\text{Li}^+$  with the inner Helmholtz plane (IHP) and outer Helmholtz plane (OHP).

$E_a$  in the four kinds of electrolytes must come from the anion adsorption layer in IHP. This work provides a clear recognition about the role of anion on Li-ion transport at the electrode/electrolyte interface and a guiding significance on development of aqueous electrolyte systems.

#### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

#### CRediT authorship contribution statement

**Jiangtao Hu:** Conceptualization, Investigation, Writing - original draft. **Wenju Ren:** Methodology. **Xin Chen:** Formal analysis. **Yiwei Li:** Investigation. **Weiyuan Huang:** Investigation. **Kai Yang:** Investigation. **Luyi Yang:** Investigation. **Yuan Lin:** Methodology. **Jiixin Zheng:** Writing - review & editing. **Feng Pan:** Conceptualization, Writing - review & editing.

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#### Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.nanoen.2020.104864>.

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